

Adsorption of coloured water on activated carbon made of olive cake waste

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المخلص

استخلاص زيت الزيتون يؤدي إلى إنتاج كميات هائلة من المخلفات الصلبة والسائلة خلال عملية التصنيع كل عام. لذلك ، تهدف هذه الدراسة العملية إلى التحقق من إمكانية استخدام مخلفات عصر زيت الزيتون (الفاتوره) كمصدر طبيعي منخفض التكلفة لتحضير الكربون المنشط (AC). في هذه الدراسة تم تفحيم بقايا مطحنة زيت الزيتون الصلب عند 200 درجة مئوية وتنشيطها كيميائياً باستخدام طريقتين تشمل النموذج الأول (25% Zncl₂) والنموذج الثاني (25% Zncl₂ + 25% H₂SO₄) للتحقق من كفاءة الكربون المنشط المحضر ، تم إجراء إزالة لون صبغة Methylene Blue الموجودة في محلول مائي. تمت دراسة فعالية هذه العملية من خلال تأثيرات المعلمات الرئيسية مثل وقت التلامس ودرجة الحموضة وكمية الكربون المنشط المستخدم. أظهرت النتائج المتحصل عليها أن إزالة اللون باستخدام النموذج II كان أكثر كفاءة من النموذج الأول. القيم المثلى للأس الهيدروجيني ووقت التلامس وكمية AC كانت 5 و 120 دقيقة و 2.5 جم / لتر على التوالي. في هذه الظروف التشغيلية كان الحد الأقصى لإزالة الميثيلين الأزرق من الماء 75%. تشير النتائج إلى أن مخلفات عصر زيت الزيتون لديها إمكانية في تطبيقات معالجة المياه في المستقبل بسبب قدرتها العالية على الامتصاص.

ABSTRACT

Production of olive oil leads to generate massive amounts of olive-waste cakes during the manufacture process every year. Therefore, this experimental study aims to investigate the potential of olive-waste cake as a low-cost natural source for preparation activated carbon (AC). The solid olive oil mill residue was carbonized at 200 °C and chemically activated using two methods including Model I (25% Zncl₂) and Model II (25% Zncl₂ + 25% H₂SO₂) . To investigate the efficiency of prepared AC, decolourization of methylene blue founded in an aqueous solution was conducted. The effectiveness of this process was studied via key parameters effects such as contact time, pH, and AC dose. The achieved results showed that the decolourization using Model II was more than of Model I. The optimum values of pH, contact time, and AC dose were 5, 120 min, and 2.5 g/L respectively. At these conditions the maximum methylene blue removal was

75%. The results indicate that olive-waste cake has a potential in future water treatment applications due to its high adsorption capacity.

Keywords: Olive mill waste, activated carbon, methylene blue

1. INTRODUCTION

Colour is the most clear indicator of water pollution. These coloured waters usually originate from the textile, pulp, and paper industries. About ten thousand different dyes and over 7×10^5 tons are generated in the world every year (Pala et al., 2006). Dyes are adhered to the material structure via covalent bonds to give their colours (Bafana et al., 2011). The discharge of effluents containing dyes into water bodies can be toxic to aquatic life (Kadirvelu et al., 2003). Furthermore, light penetration through water can be decreased by dyes, leading to a lack of oxygen in water. Coloured waters are also toxic to people and might cause several diseases such as skin irritation and eye burn (Ming et al., 2015). Among these dyes, Methylene Blue is one of the most commonly used in the industry. Figure 1 shows the molecular structure of methylene blue.

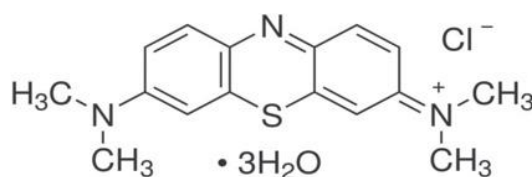


Figure 1 Molecular structure of methylene blue

The treatment of colored water is usually conducted by conventional methods such as adsorption (McKay, 1989) and biological oxidation (Paprowicz and Slodczyk, 1988).

Activated carbon adsorption can be effectively used to treat different kinds of water pollution which include dye removal (Hock et al., 2018), the removal of metallic micro pollutants, organic compounds, and pesticides (Njau et al., 2014). Activated carbon (AC) is the most promising method due to its safe use, cost-effective, and simple equipment design (Ioannidou, and Zabaniotou, 2007). However, the cost of using this technique mainly depends on the source of

activated carbon used in this process. Therefore, the use of agricultural wastes have been a significant economical solution to this issue (Toscazo et al., 2005).

Various sources of natural materials have been widely used for the industrial production of activated carbon such as coal, coconut shell, and wood (Hettiarachchi et al., 2017, Musa et al., 2019). Moreover, other agriculture by-products have been used including date stones (Girgis et al., 2002), rice husks (Chuah et al., 2005), peach stones (Ioannidou et al., 2007) and grain sorghum (Diao et al., 2002). Regarding olive-waste cakes as a source of activated carbon there have been a few studies that covered this topic (Sellami et al., 2008 and Baccar et al., 2009).

In fact, Libya is one of the largest countries in the olive oil production so there are massive amounts of olive-waste cakes generating during the manufacture process every year. In general, the olive oil production process generates about 20% of oil, 30% of waste solids, and 50% of wastewater (Chuah et al., 2005). According to (Baccar et al., 2009), the yearly average of olive-waste cakes production is about 200000 tons which can vary from country to another. Beside the use of these large amounts to produce activated carbon for water treatment purposes it can also contributes to minimizing the solid wastes in the environment.

The production of effective activated carbon depends on the nature of raw materials and the preparation method. This method includes physical and chemical procedures as well as key parameters (Suarez et al., 2002 ; Vinke et al., 1999). Drying, grinding and carbonizing are the most important steps of the physical treatment process that control the pore size and surface area of AC. For chemical procedures different chemicals have been used as a dehydrating agents such as $ZnCl_2$ only, ($ZnCl_2 + H_2SO_2$), KOH, and H_3PO_4 (Thomas and George, 2015). The general activation procedures can be categorized as shown in Figure 2 (Sellami et al., 2008).

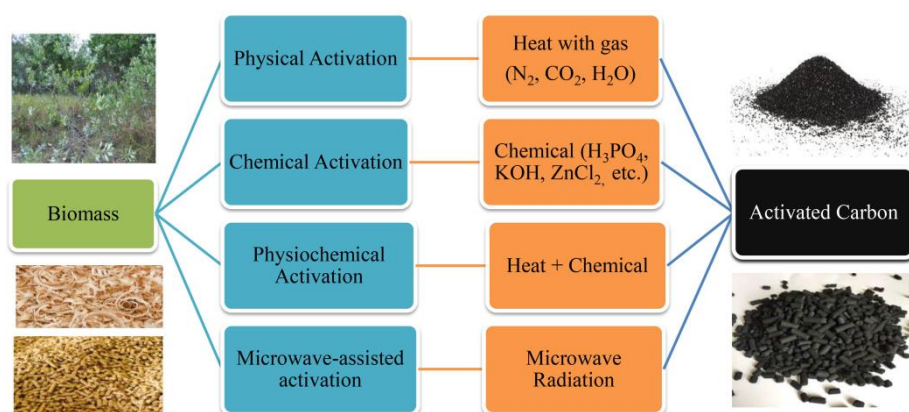


Figure 2 A general method of preparation of activated carbon from natural source.

Therefore, the present work aims to prepare activated carbon from Libyan olive-waste cakes as a natural source. Furthermore, it investigates key parameters affecting the efficiency of the production process. Finally, it examines the use of the prepared activated carbon to remove methylene blue from water.

2. MATERIALS AND METHODS

2.1 Materials and Equipment

All chemicals used in these experiments were checked for expire dates. 30 ppm of methylene blue ($C_{16}H_{18}ClN_3S$), 25% of sulphuric acid (H_2SO_4), and 25% of zinc chloride ($ZnCl_2$) were prepared. Figure 3 shows equipment used in this work including JENWAY 6300 Spectrophotometer, magnetic stirrer CAT M17.5.



Figure 3 Spectrophotometer and magnetic stirrer

2.2 Preparation of activated carbon

Olive-waste cakes were collected from an olive oil mill located in Gharyan, Libya. This solid residue was used as a raw material for the production of activated carbon. The activation method can be defined as physical and chemical processes that enormously increase carbon surface area by removing hydrocarbons (Musa et al., 2019). The process of changing the olive-waste cake into coal is called carbonization while the chemical decomposition by heating it without oxygen is called pyrolysis (Charcoal, 2014 ; Tseng et al., 2008). First of all, 500 g of olive-waste cake was washed with distilled water and dried at 200 °C for 180 min. Then the carbonized sample was crushed until it became homogeneous powder. After that the powder taken into a thermal frying pan and covered with aluminium foil. This pan was placed in the furnace at 300 °C for 3hr in order to perform the pyrolysis step. The carbonization material was again crushed to obtain smaller particles. For model I (25% of ZnCl_2) Chemical activation was performed using a mixture with the powder to make a paste. Then the mixture was placed in the furnace at 100 °C for 30 min for drying. Finally, the prepared activated carbon was washed using distilled water and filtered to obtain the final form of the activated carbon. Figure 4 shows the raw material of olive-waste cake and the prepared carbon.



Figure 4 (a) Olive-waste cake (raw material), (b) Prepared AC

All the above procedures were repeated for model II (25% of ZnCl_2 and 25% H_2SO_4). Both models were left to naturally dry for three days at room temperature.

2.3 Calibration curve of methylene blue

Stock solution of methylene blue (1000 ppm) in distilled water was prepared and stirred for 15 min for more homogeneity. Then, different concentrations (5 ppm, 15 ppm, 20 ppm, 25 ppm, 30 ppm, and 35 ppm) of methylene blue were prepared by diluting the stock solution. The absorbance of these concentrations were measured at $\lambda_{\text{max}}=664 \text{ nm}$ using UV/vis spectrophotometer (JENWAY 6300) to get the absorbance equation for various concentrations. Figure 4 shows the relation between absorbance and concentrations.

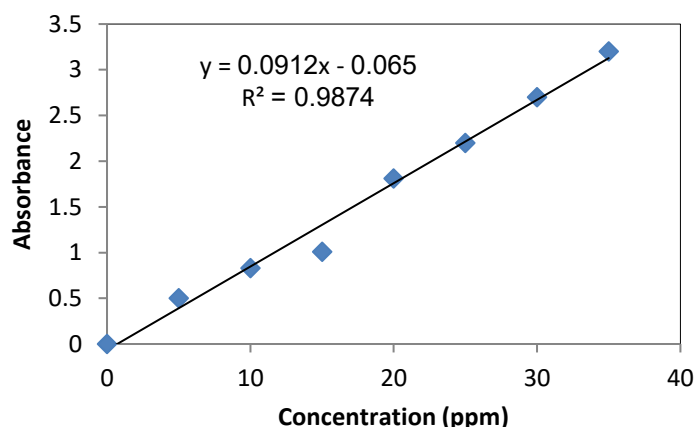


Figure 4 Calibration curve of methylene blue

2.4 Use of activated carbon (AC)

Two models of activated carbon (AC) were used to remove methylene blue from an aqueous solution at pH 7. Two grams of AC (Model I) were added to 1L of 30 ppm methylene blue sample and continuously stirred for 5 min before taking the first sample for degradation reading. Then five samples were taken at 15 min, 45 min, 90 min, 120 min, and 150 min respectively. To study the effect of pH and the initial concentration of AC the above steps were repeated for various values. Furthermore, the same procedures were implemented for AC (Model II).

3. RESULTS AND DISCUSSION

3.1 Comparison between Model I and Model II

The efficiency of methylene blue decolourization for each condition at a fixed time interval was determined. The removal percentage of the colour from wastewater was calculated using the following equation:

$$\text{Decolourization (\%)} = [(C_0 - C_e) / C_0] \times 100 \quad (1)$$

Where, C_0 and C_e are the dye concentration at initial stage and equilibrium stage respectively (ppm).

To investigate the influence of acid addition on the preparation method of AC, two models were used under the same conditions (2 g AC, pH 7, 150 min) for the decolourization of 30 ppm methylene blue. Figure 5 shows the obtained experimental results of this comparison.

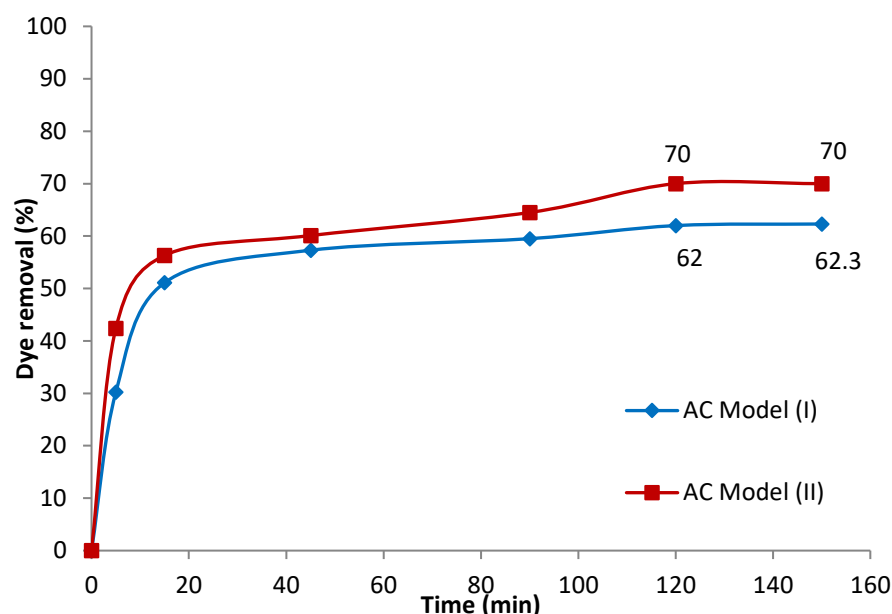


Figure 5 Comparison between AC models I & II (pH 7, 2 g/L AC, 30 ppm MB)

It can be seen that the activated carbon treated with sulfuric acid was more effective than zinc chloride alone. This result might be due to the lower total ash content of the carbon and lower water content. Acid washed activated carbon is desirable for treating drinking water and food grade applications (Bedia et al., 2020). Furthermore, the maximum decolourization for both models was at 120 min of contact time.

3.2 Effect of AC dose

The influence of the initial concentration of activated carbon on the dye removal was investigated. In this part model II was used to study this effect due to its higher efficiency compared to model I. Different initial AC doses was used at following conditions 30 ppm of methylene blue, free pH, and 150 min contact time. Figure 6 shows the obtained results and it can be clearly seen that the removal efficiency increases with increasing AC concentrations with the maximum value at 2.5 g/L. After that the decolourization percentage started to decrease which might be due to unsaturated active centers.

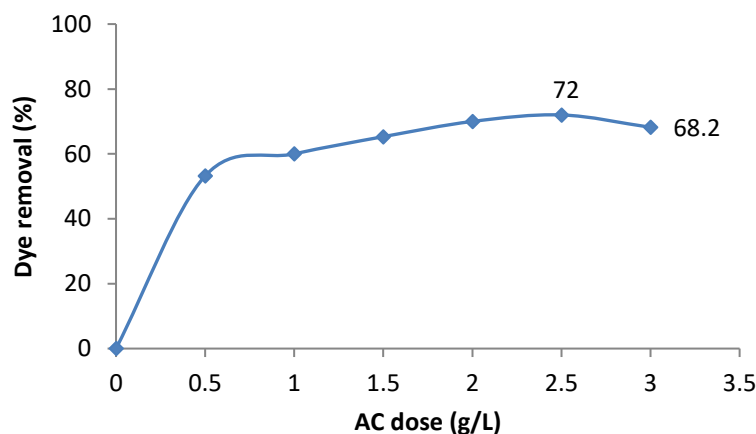


Figure 6 Effect of AC dose on methylene blue adsorption (Model II, 30 ppm MB, and 150 min)

3.2 Effect of pH

pH is a key parameter playing an important role in adsorption processes. The influence of pH on the removal of methylene blue from synthetic wastewater was investigated. The adsorption of the dye onto the surface of activated carbon is mainly affected by the surface charge in other words the value of pH. Figure 7 shows the achieved results of the pH effect on the dye adsorption onto AC (Model II) from aqueous solution.

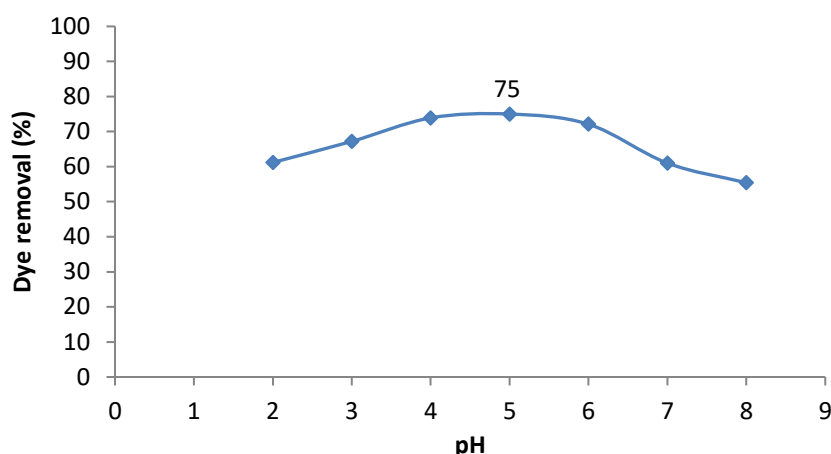


Figure 7 Influence of pH on the adsorption of 30 ppm methylene blue (2.5 g/L AC Modell II, 120 min)

It can be seen that the maximum removal efficiency was detected at pH 5, meaning the surface has a positive charge due to excess protons in the solution. It is known that the decrease in pH value leads to a rise in the H^+ concentration in the aqueous solution and the activated carbon surface gains positive charge by absorbing H^+ ions. As a result when the adsorbent surface is positively charged the dye species have a strong attraction to the positively charged of the carbon surface (Hettiarachchi et al., 2017). Above this optimum pH value, the adsorption of the dye decreased, which might be due to the weakening of the electrostatic force of attraction between the adsorbate and the adsorbent.

4. CONCLUSION

The achieved results of the present work show that the activated carbon prepared from Libyan olive-waste cake has a good potential for dye removal from aqueous solution. The chemical activation of activated carbon via zinc chloride with sulphuric acid is more effective than zinc chloride alone. The adsorption is significantly dependent on pH and the initial dose of the activated carbon. The acidic medium is found to be suitable for the dye adsorption onto the prepared activated carbon. Olive-waste cake as a natural source and low cost adsorbent of

activated carbon is promising to be efficient for other water treatments due to its high adsorption capacity.

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